Tema 4 – Termodinámica biológica Themodynamics

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Conceptos de termodinámica en biotecnología ambiental

Conservation of Energy - the First Law

- Energy balance on a bioreactor (digesters, landfills, compost)
- · Heat of metabolism
- Energy recovery

Free Energy - the Second Law

- Feasible reactions
- Thermodynamic preferences
- Relationship between free energy and yield



Energía

The capacity to do work, to make things move

Energía interna U

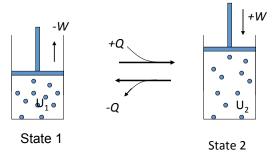
Stored or "hidden" energy. The capacity to make things move at the scale of electrons, atoms, ions and molecules.

Units of Energy:

1 calorie raises a gram of water 4.184 joules = 1 calorie 1000 calories = 1 kCal = 1 Calorie (dietary calorie)



Primera ley: Conservación de energía



$$U_1 + Q - W = U_2$$

$$-W + Q = \mathsf{U}_2 - \mathsf{U}_1 = \Delta \mathsf{U}$$





Entalpía

Enthalpy - the "heat content" of the molecules, atoms, ions in a system at constant pressure

$$H = U + PV$$

$$\Delta H = \Delta U + \Delta (PV) = \Delta U + \Delta PV + P\Delta V$$

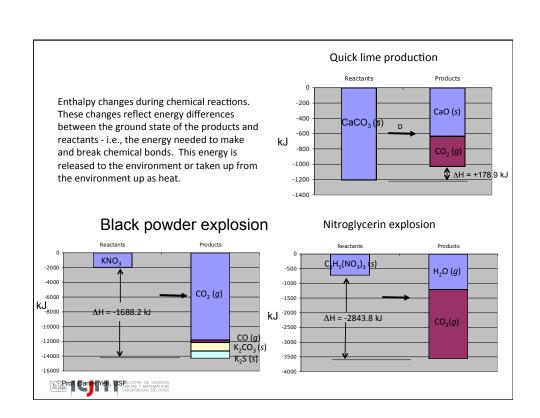
For a system at constant pressure, $\Delta P = 0$, so:

$$\Delta H = \Delta U + P\Delta V = \Delta U + W = Q$$

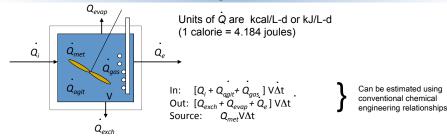
$$\Delta H = H_{\text{final}} - H_{\text{initial}}$$

 ΔH < 0 means the final state of the system has less energy than the initial state. Heat is released by the system (Q <0). This is the case for biological reactions: they are exothermic.





Balance de energía en un bioreactor



$$\begin{split} \dot{Q}_{acc} \, \mathsf{V} \Delta \mathsf{t} &= \left[\dot{Q}_i + \dot{Q}_{agit} + \, \dot{Q}_{gas} \, \right] \, \mathsf{V} \Delta \mathsf{t} - \left[\dot{Q}_{exch} + \, \dot{Q}_{evap} + \, \dot{Q}_e \, \right] \, \mathsf{V} \Delta \mathsf{t} + \, \dot{Q}_{met} \, \mathsf{V} \Delta \mathsf{t} \\ \mathsf{For steady state:} \, \dot{Q}_{acc} &= 0 = \dot{Q}_i - \dot{Q}_e + \dot{Q}_{agit} + \, \dot{Q}_{gas} - \dot{Q}_{exch} - \dot{Q}_{evap} + \dot{Q}_{met} \\ & 0 = \mathsf{Q}^{\circ} \mathsf{C}_{\mathsf{p}} [\mathsf{T}_i - \mathsf{T}_e] + \dot{Q}_{agit} + \, \dot{Q}_{gas} - \dot{Q}_{exch} - \dot{Q}_{evap} + \dot{Q}_{met} \end{split}$$

Can solve this for $T_{\rm e.}$ $C_{\rm p}$ = heat capacity of water

For non-steady state $Q_{acc} = c_{p,sys}\Delta T/\Delta t~$ where $c_{p,sys}$ is the overall heat capacity of the system [kJ/L-°C].

What is Q_{met} ?

Q_{met} = \(\times H\)\text{met} [kcal/g] x volumetric rate of consumption of substrate [g/L-d]

Dos formas para estimar la entalpía del metabolismo (ΔH_{met})

1. Compute from balanced reaction for conversion of reactants, r, to products, p:

$$\begin{split} &a_{1}r_{1}+a_{2}r_{2}+...a_{n}r_{n} \Longrightarrow b_{1}p_{1}+b_{2}p_{2}+...b_{m}p_{m} \\ &\Delta H_{\textit{met}} = \sum_{i=1}^{m} b_{i}H_{p,i} - \sum_{i=1}^{n} a_{i}H_{r,i} \end{split}$$

where $H_{p, 1}$ = standard enthalpy of products, $H_{r, 1}$ = standard enthalpy of reactants

Uses standard molar enthalpy data Not useful for mixed substrates.

Requires an estimate of the molar enthalpy of biomass H_{biomass} Estimated at -3.72 kJ/g vss (Roels, 1980)

2. Estimate from heat of combustion data

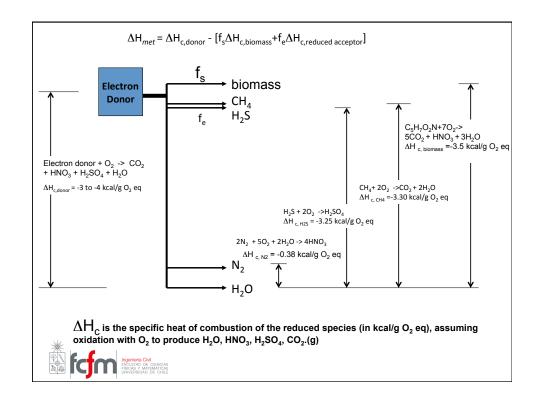
ASSUMPTION: Heat of metabolism = heat released by combustion of electron donor minus the heat released by combustion of the reduced products of metabolism (biomass + reduced electron acceptor).

$$\Delta H_{met} = \Delta H_{c,donor} - \left[f_s \Delta H_{c,biomass} + f_e \Delta H_{c,reduced\ acceptor} \right]$$

 ΔH_c =heat of combustion



Entalpía de combustión ∆Hc para algunas substancias*				
Carbohydrates glucose	<u>kcal/g</u> -3.74	<u>kcal/g O₂ eq</u> -3.51		
Fats palmitic acid tripalmitin	-9.37 -9.28	-3.26 -3.24		
Protein glycine (amino acid)	-2.18	-3.41		
Hydrocarbons decane methane	-11.34 -13.18	-3.25 -3.30		
Biomass -6.9 -3.5 Hydrogen -34.2 -4.27 * Assumes combustion with O ₂ to CO ₂ (g), H ₂ O(l), HNO ₃ (aq)				



Composting

Aerobic Thermophilic Degradation

- Stabilization
 - o Reduce odors
 - o Decrease rate of decay
- Decrease mass
- Reduce pathogens

<u>Disadvantages</u> Area intensive

Costly - labor intensive Incomplete disinfection





Composting Windrows

Composting

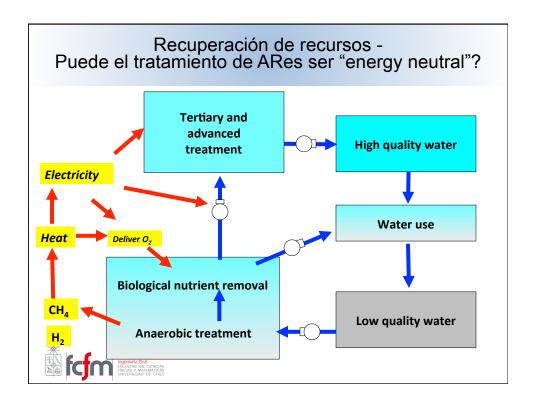
The heat of combustion (~3.4 kcal/g COD) from decay aids in drying the compost

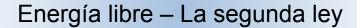


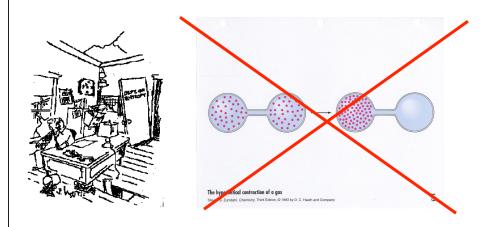
Water vapor rising from compost piles with forced aeration



Biogenic methane gas can be recovered from landfills and burned for energy ENGINE LANDFILL GAS BURNING UNDERGROUND PIPES BLOWER BLOWER Http://www.lann-arbor.mi.us/PublicServices/FieldOperations/SolidWaste/education/rrc/landfill.html







In the absence of outside energy inputs, energy flows from being concentrated in one place to diffuse and spread out. $\Delta S_{univ} > 0$ for any change.



Energía libre y Entropía (S)

For a given macrostate (V, T, P, composition), he number of microstates is a measure of S. Microstates are specific configurations of energy within a molecules or a system of molecules.

 $\frac{\text{Think of temperature T} \text{ as a measure of the average energy per microstate}}{\text{If we add an amount of energy } Q \text{ to a system at constant temperature, the}}$

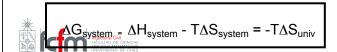
number of microstates will change by Q/T, so $\Delta S_{system} = \frac{Q}{T}$

$$\Delta H_{\text{system}} = Q_{\text{system}} = -Q_{\text{environment}}$$

so
$$\Delta S_{environment} = -\frac{\Delta H_{system}}{T}$$

$$\Delta S_{univ} = \Delta S_{system} + \Delta S_{environment}$$

$$\Delta S_{univ} = \Delta S_{system} - \frac{\Delta H_{system}}{T}$$



Energía libre y Equilibrio

$$a_1r_1 + a_2r_2 + ...a_nr_n \rightarrow b_1p_1 + b_2p_2 + ...b_mp_m$$

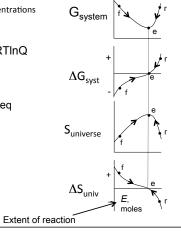
Standard conditions (25°C, all concentrations =1 M or 1 atm)

$$\Delta G^{\circ} = \sum_{i=1}^{m} b_{i} G_{p,i}^{o} - \sum_{i=1}^{n} a_{i} G_{r,i}^{o}$$
Actual measured concentrations

$$\Delta G = \Delta G^{\circ} + RTIn \left[\frac{\left(p_{1} \right)^{b_{1}} \left(p_{2} \right)^{b_{2}} ... \left(p_{m} \right)^{b_{m}}}{\left(r_{1} \right)^{a_{1}} \left(r_{2} \right)^{a_{2}} ... \left(r_{n} \right)^{a_{n}}} \right] = \Delta G^{\circ} + RTInQ$$

When $\Delta G = 0$, then $\Delta G^{\circ} = -RTInQ_{eq}$

 $Q_{eq} = K = equilibrium constant$





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El proceso Haber:

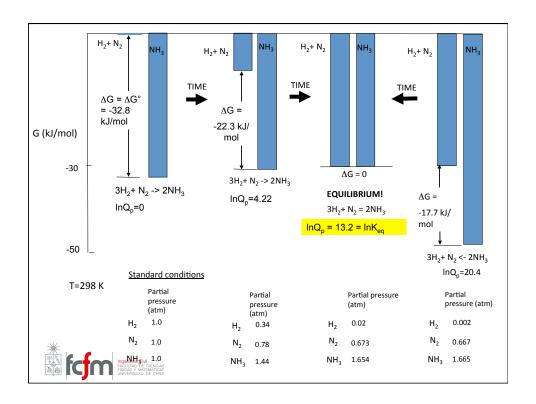
$$3H_2 + N_2 = 2NH_3$$

$$\Delta G = \Delta G^{\circ} + RTInQ_{p}$$

$$\mathbf{Q_p} = \frac{P_{\text{NH}_3}^2}{P_{\text{H}_2}^3 P_{\text{N}_2}}$$

$$K_{eq} = e^{13.2}$$
 @ 25°C



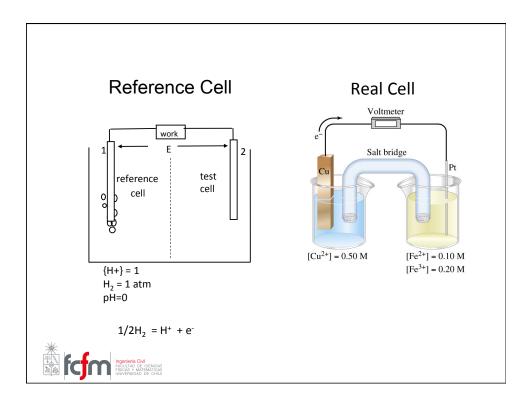


Energía libre y Voltaje

Nernst equation $\Delta G = -nFE$ n = number of electron equivalents transferred F = Faraday's constant (96,493 coulombs/eq)

Free energy per mole of electrons is directly proportional to voltage. The proportionality constant is Faraday's constant.





Reacciones factible

Standard half reaction reduction potentials for electrode reactions at 25°C (from Bockris and Reddy, 1977)

Electrode reaction	E°, V	Electrode reaction	E°, V
Li ⁺ + e ⁻ = Li	-3.01	Cd ²⁺ + 2e ⁻ = Cd	-0.40
$Rb^+ + e^- = Rb$	-2.98	In ³⁺ + 3e ⁻ = In	-0.34
$Cs^+ + e^- = Cs$	-2.92	Ti ⁺ + e ⁻ = Ti	-0.34
$K^+ + e^- = K$		Co ²⁺ + 2e ⁻ = Co	-0.27
Ba ²⁺ + 2e ⁻ = Ba	-2.92	Ni ²⁺ + 2e ⁻ = Ni	-0.23
$Sr^{2+} + 2e^{-} = Sr$	-2.89	Sn ²⁺ + 2e ⁻ = Sn	-0.14
$Ca^{2+} + 2e^{-} = Ca$	-2.84	Pb ²⁺ + 2e ⁻ = Pb	-0.13
Na ⁺ + e ⁻ = Na	-2.71	$D^+ + e^- = 0.5D_2$	-0.003
Mg ²⁺ + 2e ⁻ = Mg	-2.38	$H^+ + e^- = 0.5H_2$	0.00
Ti ²⁺ + 2e ⁻ = Ti	-1.75	Cu ²⁺ + 2e ⁻ = Cu	0.34
$Be^{2+} + 2e^{-} = Be$	-1.70	$0.5O_2 + H_2O + 2e^- = 2OH^-$	0.40
Al 3+ + 3e = Al	-1.66	Cu ⁺ + e ⁻ = Cu	0.52
$V^{2+} + 2e^{-} = V$	-1.50	Hg ²⁺ + 2e ⁻ = Hg	0.80
$Mn^{2+} + 2e^{-} = Mn$	-1.05	$Ag^+ + e^- = Ag$	0.80
$Zn^{2+} + 2e^{-} = Zn$		Pb ²⁺ + 2e ⁻ = Pb	0.83
Ga ³⁺ + 3e ⁻ = Ga		Ir ³⁺ + 3e ⁻ = Ir	1.00
Fe ³⁺ + 3e ⁻ = Fe	-0.44	$O_2 + 4H^+ + 4e^- = 2H_2O$	1.23

How could you design a system to remove copper from solution?



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Combustibles (donadores de e-)

Organic molecules are good fuels. For CO_2 /organic molecule couples, $E^{\circ \prime}$ <0 (so they are >0 when the organic is oxidized to CO_2). When coupled to reduction half reactions for oxidants, the resulting whole reactions have positive voltages E >0.

Some inorganics are also good fuels:

best

worst

e donor	Half reaction	E°' (V)
HSO ₃	$SO_4^{2-} + 3H^+ + 2e^- = HSO_3^- + H_2O$	-0.51
H ₂	$2H^{+} + 2e^{-} = H_{2}$	-0.41
S ₂ O ₃ ²⁻	$2SO_4^{2-} + 10H^+ + 8e^- = S_2O_3^{2-} + 5H_2O$	-0.25
HS ⁻	$SO_4^{2-} + 9H^+ + 8e^- = HS^- + 4H_2O$	-0.22
S	$SO_4^{2-} + 8H^+ + 6e^- = S + 4H_2O$	-0.20
AsO ₃ ³⁻	$AsO_4^{3-} + 4H^+ + 2e^- = H_2AsO_3^- + H_2O$	+0.15
Cu⁺	$Cu^{2+} + e^{-} = Cu^{+}$	+0.16
Se	$SeO_4^{2-} + 8H^+ + 6e^- = Se + 4H_2O$	+0.33
NH ₄ ⁺	$NO_3^- + 10H^+ + 8e^- = NH_4^+ + 3H_2O$	+0.36
Mn (II)	$MnO_2 + 4H^+ + 2e^- = Mn^{2+} + 2H_2O$	+0.47
Fe (II)	$Fe^{3+} + e^{-} = Fe^{2+}$	+0.77



Oxidantes (receptores de e-)

best

e acceptor	Half reaction	E°' (V)
N ₂ O	$N_2O + 2H^+ + 2e^- = N_2 + H_2O$	+1.31
CIO ₃ -	$CIO_3^- + 6H^+ + 6e^- = CI^- + 3H_2O$	+1.04
NO ₂ -	$2NO_2^- + 8H^+ + 6e = N_2 + 4H_2O$	+0.94
O ₂ Fe ³⁺	$O_2 + 4H^+ + 4e^- = 2H_2O$	+0.82
Fe ³⁺	$Fe^{3+} + e^{-} = Fe^{2+}$	+0.77
NO ₃	$2NO_3^- + 12H^+ + 10e^- = N_2 + 6H_2O$	+0.74
NO ₃	$NO_3^- + 2H^+ + 2e^- = NO_2^- + H_2O$	+0.43
NO ₃	$NO_3^- + 10H^+ + 8e^- = NH_4^+ + 3H_2O$	+0.36
C ₆ H ₄ CICOO ⁻	$C_6H_4CICOO^- + H^+ + 2e^- = C_6H_5COO^- + CI^-$	+0.26
(CH ₃) ₂ SO	$(CH_3)_2SO + 2H^+ + 2e = (CH_3)_2S + H_2O$	+0.23
$S_2O_3^{2-}$	$S_2O_3^{2-} + 8H^+ + 8e^- = 2HS^- + 3H_2O$	-0.21
SO ₄ ² -	$SO_4^{2-} + 9H^+ + 8e^- = HS^- + 4H_2O$	-0.22
CO ₂	$CO_2 + 8H^+ + 8e = CH_4 + 2H_2O$	-0.24
S	S + H ⁺ + 2e ⁻ = HS ⁻	-0.27

worst



Energía libre y Yield

Why do some microorganisms have a lower yield than others?

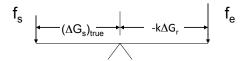
Microorganisms "prefer" to convert all their substrate into biomass ($f_s = 1.0$), but some substrate must be burned to give energy for synthesis.

When energy reactions yield very little energy per equivalent, most of the electrons must be used to produce energy for cell synthesis (f_e must be large). For these reactions, f_s and yield will be small.

Other energy reactions generate considerable energy per equivalent. Fewer equivalents can generate sufficient energy for cell synthesis (f_e can be small). For these reactions, f_s and yield will be large.



Balance de energía libre de McCarty y fs



For a balance to be achieved, $f_s(\Delta G_s)_{true} = -f_e k \Delta G_r$

 ΔG_s = Energy required to synthesize one eq of cells from a carbon source

 $\Delta G_{\mbox{\tiny r}}$ = Energy obtained by combining the electron donor and acceptor



$$\begin{split} &f_s (\Delta G_s)_{true} = -f_e k \Delta G_r &f_e = 1 - f_s \\ &f_s \left(\Delta G_s \right)_{true} = -k \Delta G_r + f_s k \Delta G_r \\ &f_s \left(\Delta G_s \right)_{true} - f_s k \Delta G_r = -k \Delta G_r \\ &f_s \left[\left(\Delta G_s \right)_{true} - k \Delta G_r \right] = -k \Delta G_r \\ &f_s = \frac{-k \Delta G_r}{-k \Delta G_r} + \left(\Delta G_s \right)_{true} \end{split}$$



For synthesis, assume that carbon from the donor is converted to pyruvate then to the cell.

$$\left(\!\Delta G_{_S}\right)_{\!true} \,=\, \frac{\Delta G_{_p}}{k^m} \,+\, \frac{\Delta G_{_{\!pc}}}{k} \quad \begin{array}{ll} m = -1 \text{ if } \Delta G_{_p} < 0 \\ m = +1 \text{ if } \Delta G_{_p} > 0 \end{array}$$

 ΔG_{p} = Energy required to convert the carbon source to pyruvate

 ΔG_r = Energy required to convert pyruvate carbon to cells



Estimación of fs Superscript indicates that this

f_s is a maximum value (I.e., no decay)

Electron donor: acetate Electron acceptor: nitrate N source: nitrate

ΔG°'(kJ/eq)

$$R_d$$
: $\frac{1}{8}CH_3COO^- + \frac{3}{8}H_2O = \frac{1}{8}CO_2 + \frac{1}{8}HCO_3^- + H^+ + e^-$ -27.40 (as written)

$$R_a$$
: $\frac{1}{5}NO_3^- + \frac{6}{5}H^+ + e^- = \frac{1}{10}N_2 + \frac{3}{5}H_2O$ -72.20

 ΔG_r = Energy released = -27.40-72.20 = -99.62 KJ/eq



Energy required for synthesis = $\Delta G_p + \Delta G_{pc}$

 ΔG_p is obtained by combining R_d with the pyruvate half reaction:

$$\frac{1}{5}CO_2 + \frac{1}{10}HCO_3^- + H^+ + e^- = \frac{1}{10}CH_3COCOO^- + \frac{2}{5}H_2O \qquad \frac{\Delta G^{o'}(kJ/eq)}{+35.09}$$

$$\Delta G_p$$
=-27.40+(+35.09)=7.69 KJ/eq

Assume k=0.6, ΔG_{pc} =13.4 kJ/eq for nitrate N source

$$f_s^{\circ} = \frac{-k\Delta G_r}{-k\Delta G_r + \frac{\Delta G_{pc} + \Delta G_p}{k}} = \frac{-0.6(-99.60)}{-0.6(-99.60) + \frac{13.4 + 7.69}{0.6}} = 0.63$$



$$Y = 0.63 \frac{4.04^{\circ} g^{\circ} vs/eq}{\left(\frac{1}{8}\right) 59^{\circ} g^{\circ} acetate/eq} = \frac{0.35^{\circ} gvs}{g^{\circ} acetate}$$

Energía libre de formación

- ΔG_f° = Free energy of formation, under standard conditions (pH7, 25°C, all reactants at 1M)
 - if <u>negative</u>, reaction is energy yielding and will proceed favorably (**exergonic**)
 - if <u>positive</u>, reaction is energy consuming and will <u>not</u> proceed favorably (endergonic)



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Energía libre de reacción

- ΔG° = Free energy of reaction, under standard conditions (pH7, 25°C, all reactants at 1M)
 - if <u>negative</u>, reaction is energy yielding and will proceed favorably (**exergonic**)
 - if <u>positive</u>, reaction is energy consuming and will <u>not</u> proceed favorably (endergonic)



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Reacciones medias REDOX de Nitrogen

EXAMPLE 15.8. Predicting products of redox reactions involving nitrogen

In certain laboratory procedures it is necessary to remove NH₄ ions from solution. This is accomplished by heating the solution with concentrated nitric acid and evaporating to dryness. Write a balanced net ionic equation for this reaction.

Solution. Table 15.3 informs us that ammonium ions are generally oxidized to N_2 . It also states that concentrated nitric acid is a good oxidizing agent, and is reduced to $NO_2(g)$. The two half-reactions are therefore

Oxidation $2NH_4^+ \rightarrow N_2(g) + 6e^- + 8H^+(aq) -3 0$

Reduction $2H^{+}(aq) + NO_{3}^{-} + e^{-} \rightarrow NO_{2}(g) + H_{2}O_{+}$

The correctly balanced overall equation is therefore

 $2NH_4^+ + 6NO_3^- + 4H^+(aq) \rightarrow 6NO_2(g) + N_2(g) + 6H_2O$

EXAMPLE 15.9. The disproportionation of nitrous acid

Balance the equation for the disproportionation of nitrous acid.

Solution. The two half-reactions are

Oxidation $HNO_2 + H_2O \rightarrow NO_3^- + 2e^- + 3H^+(aq)$

Reduction $H^{+}(aq) + HNO_{2} + e^{-} \rightarrow NO(g) + H_{2}O$ +3 +2

Segal, Chemistry: experiment and theory. 1985