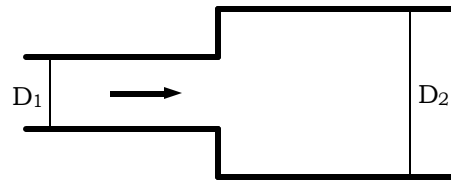


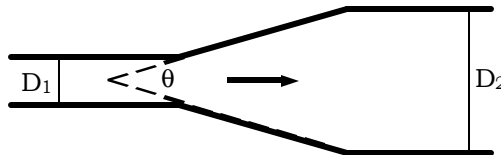
## PÉRDIDAS SINGULARES EN TUBERÍAS

### ENSANCHE BRUSCO

$$\Lambda = k \frac{v_1^2}{2g}, \quad k = (1 - \beta^2)^2, \quad \beta = \frac{D_1}{D_2}$$



### ENSANCHE PAULATINO



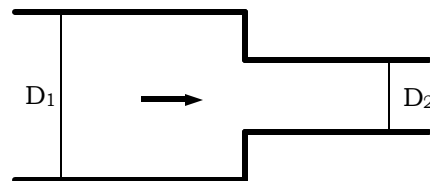
$$\begin{aligned} \theta < 45^\circ \quad Re_1 < 4000 \quad k &= 5,2(1 - \beta^4) \operatorname{sen}\left(\frac{\theta}{2}\right) \\ Re_1 > 4000 \quad k &= 2,6(1 + 3,2f_1)(1 - \beta^2) \operatorname{sen}\left(\frac{\theta}{2}\right) \end{aligned}$$

$$\begin{aligned} 45^\circ < \theta < 180^\circ \quad Re_1 < 4000 \quad k &= 2(1 - \beta^4) \\ Re_1 > 4000 \quad k &= (1 + 3,2f_1)(1 - \beta^2) \end{aligned}$$

$f_1$  es el factor de fricción de la tubería con diámetro  $D_1$

### CONTRACCIÓN BRUSCA

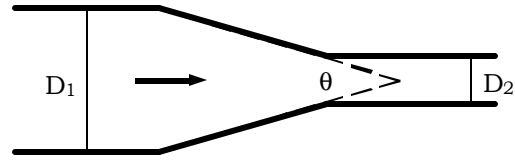
$$\begin{aligned} Re_1 < 2500 \quad k &= \left(1,2 + \frac{160}{Re_1}\right)(\beta^4 - 1) \\ Re_1 > 2500 \quad k &= (0,6 + 0,8f_1)(\beta^2 - 1)\beta^2 \end{aligned}$$



### CONTRACCIÓN REDONDEADA

$$k = \left(0,1 + \frac{50}{Re_1}\right)(\beta^4 - 1)$$

## CONTRACCIÓN PAULATINA



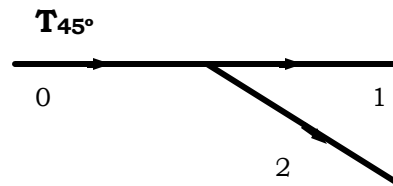
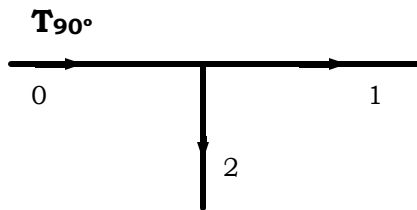
$$\begin{aligned} \theta < 45^\circ \quad Re_1 < 2500 \quad k &= 1,6 \left( 1,2 + \frac{160}{Re_1} \right) (\beta^4 - 1) \text{sen} \left( \frac{\theta}{2} \right) \\ Re_1 > 2500 \quad k &= 1,6 (0,6 + 1,92f_1) \beta^2 (\beta^2 - 1) \text{sen} \left( \frac{\theta}{2} \right) \end{aligned}$$

$$\begin{aligned} 45^\circ < \theta < 180^\circ \quad Re_1 < 2500 \quad k &= \left( 1,2 + \frac{160}{Re_1} \right) (\beta^4 - 1) \sqrt{\text{sen} \left( \frac{\theta}{2} \right)} \\ Re_1 > 2500 \quad k &= (0,6 + 1,92f_1) \beta^2 (\beta^2 - 1) \sqrt{\text{sen} \left( \frac{\theta}{2} \right)} \end{aligned}$$

## DERIVACIONES

$$\Lambda_{0-1} = k_1 \frac{v_0^2}{2g}$$

$$\Lambda_{0-2} = k_2 \frac{v_0^2}{2g}$$



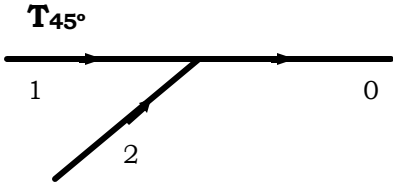
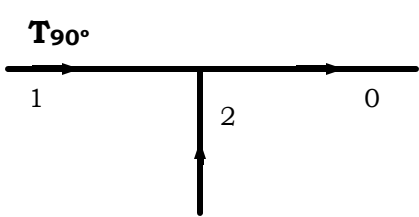
|                  |           |      |      |      |      |      |      |
|------------------|-----------|------|------|------|------|------|------|
|                  | $Q_1/Q_0$ | 0,0  | 0,2  | 0,4  | 0,6  | 0,8  | 1,0  |
|                  | $Q_2/Q_0$ | 1,0  | 0,8  | 0,6  | 0,4  | 0,2  | 0,0  |
| T <sub>90°</sub> | $k_1$     | 0,40 | 0,35 | 0,20 | 0,10 | 0,05 | 0,05 |
|                  | $k_2$     | 1,30 | 1,10 | 0,96 | 0,90 | 0,88 | 0,96 |
| T <sub>45°</sub> | $k_1$     | 0,45 | 0,40 | 0,25 | 0,15 | 0,10 | 0,08 |
|                  | $k_2$     | 0,35 | 0,30 | 0,33 | 0,47 | 0,66 | 0,90 |

Todos las tuberías son de igual diámetro

CONFLUENCIAS

$$\Lambda_{1-0} = k_1 \frac{v_0^2}{2g}$$

$$\Lambda_{2-0} = k_2 \frac{v_0^2}{2g}$$



|                |           |      |      |      |      |      |      |
|----------------|-----------|------|------|------|------|------|------|
|                | $Q_1/Q_0$ | 0,0  | 0,2  | 0,4  | 0,6  | 0,8  | 1,0  |
|                | $Q_2/Q_0$ | 1,0  | 0,8  | 0,6  | 0,4  | 0,2  | 0,0  |
| $T_{90^\circ}$ | $k_1$     | 0,60 | 0,50 | 0,40 | 0,30 | 0,18 | 0,05 |
|                | $k_2$     | 0,91 | 0,72 | 0,47 | 0,30 | 0,10 | 0,00 |
| $T_{45^\circ}$ | $k_1$     | 0,60 | 0,50 | 0,40 | 0,30 | 0,18 | 0,05 |
|                | $k_2$     | 0,50 | 0,40 | 0,25 | 0,20 | 0,10 | 0,00 |

